Sheffield Gardens SPDES Permit & WWTP Engineer's Report

NYS Route 17k Town of Montgomery Orange County, NY 12549

PREPARED BY

Pitingaro & Doetsch Consulting Engineers, P.C.

15 Industrial Drive, Suite 2 Middletown, NY 10941

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I. INTRODUCTION

MILR, LLC has contracted Pitingaro & Doetsch Consulting Engineers, PC (P&D) to prepare an Engineer's Report and the design of a new wastewater treatment plant (WWTP) to serve the Sheffield Gardens project. A location map of the project is in **Appendix A.**

The project is located at NYS Route 17k (SBLs 29-1-5.1, 5.2, 5.3, 5.4 & 5.5) in the Town of Montgomery, Orange County, NY. The total area of the site is 53.08 acres. The site is located in the RA-1, RM-1, and B-2 zoning districts. The site will be used for open space, multi-family dwellings, and the WWTP. The existing uses of the site are vacant and single-family residential. The project proposes a facility that will serve multiple users for a mixed-use development, including 225 two-bedroom apartment units, 36 one-bedroom units and 31,000 sf of potential retail space. The development will comprise a population of approximately 625 people and therefore require wastewater treatment. All proposed facilities are to be serviced by central water and central sewer. There are three (3) existing drilled wells on site.

With this project comes a demand for and use of water. The nearest WWTP is the Village of Montgomery Sewage Treatment Plant about 2 miles to the west of the site. In 2021, the plant treated and discharged a daily average of 254,000 gallons per day (gpd). The existing SPDES permit flow limit for the plant is 0.75 million gallons per day (mgd). The new incoming flow could result in failure or permit limit excursions at the existing plant. It is also undesirable to pump the wastewater 2 miles west to the Village of Montgomery Sewage Treatment Plant; the topography will not support gravity sewers. Furthermore, the Village has rejected outside users. Thus, the only practical option is to design a new WWTP to serve Sheffield Gardens. The site is in the Town of Montgomery Sewer District No. 3.

The total proposed wastewater design flow is calculated to be 56,360 gpd. To treat this incoming flow, the new WWTP will consist of a 6,730-gallon tank for anoxic treatment, four (4) Kubota membrane bioreactor (MBR) units for nutrient removal and a UV disinfection system. To hold the MBR units, there will be two (2) MBR tanks total with a capacity of 8,387 gallons each. There will be a 12,000-gallon septic tank outside of the WWTP building to be buried underground as an equalization tank. The new WWTP will be capable of treating 58,000 gpd of sewage and 98.4 lbs of BOD loading.

The effluent will be discharged in a nearby tributary creek of Wallkill River (Water Index Number: H-139-13-20 thru 53) via a large wetland adjacent to the site that drains to the culvert crossing of NYS Route 17k. **Appendix B** shows the overall plan for the site. A SPDES permit will be needed to discharge into the wetland.

This report is prepared to seek the approval of plans for the facility from the New York State Department of Environmental Protection (NYSDEC).

2. FLOW CALCULATION & WASTEWATER CHARACTERIZATION

Table 1 summarizes the proposed Sheffield Gardens facilities and their design flows. The 2014 New York State Design Standards for Intermediate Sized Wastewater Treatment Systems (2014 Standards) was used as design guidance. The total sewage flow is calculated to be 56,360. Given that there is no significant loss during the treatment process, we are proposing a discharge of 58,000 gpd of treated sanitary sewage for the SPDES permit.

No. **Facility** gpd 1 225 two-bedroom units 49,500 2 36 one-bedroom units 3,960 3 35-employee, 30,000 sf of potential retail 3,625 4 20% Reduction for Commercial Use water -725 saving fixtures Total 56,360 **Proposed SPDES** 58,000

Table 1. Sheffield Gardens Flow Calculation

The project will generate approximately 56,360 gpd of wastewater. As demonstrated by the flows in **Table 1**, approximately 95% of the Sheffield Gardens flow will be residential.

According to the 2014 New York State Design Standards for Intermediate Sized Wastewater Treatment Systems, the most important characteristics in the sewage are biological oxygen demand (BOD₅), total suspended solids (TSS), and fats, oils, and grease (FOG). Total phosphorus (TP) and ammonia (NH₄) are only considered in special cases. Nitrogen (N) and phosphorus (P) will be addressed in this case. The typical influent concentrations of these parameters are summarized in **Table 2**.

 Parameter
 Residential Sewage Range
 Residential Sewage Median

 BOD₅
 155 – 286
 220.5

 TSS
 155 – 330
 242.5

9.0

8.5

6 - 12

4 - 13

Table 2. Typical Concentrations (mg/L) of Residential Sewage Characteristics

Based on the parameters summarized in **Table 2** and influent flow data, the following flow conditions in mgd were used for the preliminary design of the MBR plant. **Table 3** displays the design flow conditions.

TP

NH₄-N

Condition Flow Unit Average Daily Flow 0.058 mgd Max. Monthly Flow 0.058 mgd Peak Daily Flow 0.11 mgd (assumed) Peak Hourly Flow 157.1 gpm (assumed)

Table 3. Design Flow Conditions

The assumed peak influent hourly flow of the MBR plant is about 157 gallons per minute (gpm) with a peak daily flow of 0.11 million gallons per day (mgd). According to the 2014 Recommended Standards for Wastewater Facilities, a population of 625 would have a peaking factor of about 3.9. The peaking factor is the ratio of peak hourly flow/design average flow. The equation below was used to estimate the peak hourly flow.

$$Peaking Factor = \frac{Peak \ Hourly \ Flow}{Design \ Average \ DailyFlow}$$
$$3.9 = \frac{Peak \ Hourly \ Flow}{0.058 \ MGD}$$
$$Peak \ Hourly \ Flow = 0.2262 \ MGD$$
$$\frac{0.2262 \ MGD}{1440 \ minutes} \times 1,000,000 = 157.1 \ gpm$$

After determining the wastewater flow and characteristics, the organic loading and solid loading on the proposed WWTP are computed to be 98.4 lbs BOD₅/day and 108.2 lbs TSS/day. Organic loading and solid loading from the potential retail space is negligible as approximately 95% of the flow is residential. The calculation details are shown in **Table 4**.

Table 4. Sheffield Gardens BOD & TSS Loadings Calculation

No.	Facility	Flow	mg BOD ₅	lb BOD5/day	mg TSS/L	lb TSS/day
140.	1 acmry	(gpd)	/L	10 BOD 57 day	mg 100/L	10 100/ day
1	225 two-bedroom	49,500	220.5	91.1	242.5	100.2
1	units	49,300	220.3	91.1	242.3	100.2
2	36 one-bedroom	3,960 220	220.5	7.3	242.5	8.0
	units	3,200	220.3	7.5	242.3	0.0
Total		-	-	98.4	-	108.2
	Average	-	220.5	-	242.5	-

3. SPDES PERMIT & PROPOSED TREATMENT PROCESS

The proposed SPDES permit anticipates 58,000 gpd of flow to be discharged into the wetland leading to a tributary creek of Wallkill River, approximately 1,500 feet east of the WWTP. The creek is a Class C waterbody that continues north to meet the Wallkill River. It is not a trout stream. **Appendix C** shows the SPDES permit application for the project. The SPDES permit has information about the flow, water quality, and discharge location.

To manage the anticipated flows, Kubota Membrane USA has prepared a preliminary design based around their SP400 Submerged Membrane Unit (SMU). The SP series was developed to create an SMU that is more energy efficient and faster to assemble on-site than the previous models while still maintaining the reliable and simple operation that is a characteristic of Kubota's MBR systems. The new WWTP will consist of a 6,730-gallon tank for an anoxic treatment, four (4) Kubota membrane bioreactor (MBR) units for nutrient removal and a UV disinfection system. A 12,000-gallon septic tank for primary settling will be outside the building, where wastewater will flow to before being processed in the MBR units. There will be two (2) tanks to hold the four (4) MBR units. **Table 5** describes the MBR system components and specifications.

Table 5. Membrane Equipment Specifications

Component	MBR Specifications
Membrane Model	SP225
Membrane Surface Area per Unit	$2,422 ft^2$
Design MLSS* at MBR	11,000 mg/L
Number of Membrane Tanks	2 Tanks
Total Number of Submerged Membrane Units	4 units (2 units per tank)
Minimum Wastewater Temperature	10 °C

^{*}Mixed liquor suspended solids

Preliminary tank sizing was performed using Kubota standard design parameters. It was based on the minimum temperature, and the maximum monthly flow and loading. Tank dimensions are included in **Table 6** below.

Table 6. Tank Dimensions and Hydraulic Retention Times

Tank Name	Dimensions (L x W)	SWD	Volume per Tank	Number of Tanks	Total Tank Volume	HRT at MMF*
Anoxic	10' x 20'	6'	6,730 gal	1	6,730 gal	3 hrs
MBR	10' x 10'	10.5'	8,387 gal	2	16,774 gal	7.6 hrs
Total	-	-	-	-	23,500 gal	10.6 hrs

^{*}Hydraulic Retention Time at Maximum Monthly Flow

4. PROPOSED TREATMENT PROCESS

Kubota is proposing an MLE process flow for the system in order to remove BOD and nitrogen. The MLE process makes use of the carbon found in the influent to treat the sludge, eliminating the need to use other carbon-based chemicals such as methanol or acetate. The proposed MBR system includes a primary settling tank and one process train with an anoxic tank and two MBR tanks operating in parallel. The system shall be capable of treating the daily design wastewater flow to <30 mg/L BOD and <30 mg/L TSS. A feed forward pump will be used to pump flow up to the MBR so that it can return by gravity to the anoxic tank. **Appendix E** displays the flow diagram of the proposed treatment process. The details of the blower, tanks, MBR units, and associated equipment are shown in **Appendix F**.

The dimensions of the WWTP building will be 24' x 38' to accommodate the tanks and equipment. The 12,000-gallon septic tank will be outside the WWTP building. **Appendix D** displays the WWTP layout.

The invert depth at the last sewer stub connecting the facilities into the WWTP is 395.0 ft. The discharge will flow south out of the WWTP building around the DEC wetland boundaries and neighboring property (29-6-1) and then east to discharge into the wetland (Wetland ID WD-29) that is connected to the tributary of Wallkill River.

4.1. Primary Settling Tank

For a proposed SPDES flow of 58,000 gpd, a 12,000-gallon septic tank is recommended before processing in the MBR units. The tank will be outside of the WWTP building and underground. **Table 7** summarizes the specifications of the tank.

Parameter	Value	Unit	Reference
Total Volume	12,000	gallon	Proposed tank capacity
Influent BOD ₅ Conc.	220.5	mg/L	
Influent TSS Conc.	242.5	mg/L	Determined in Table 4
Influent P Conc.	10	mg/L	
Estimated Effluent BOD ₅ Conc.	154.35	mg/L	30% removal, 2002 EPA OWTS Manual
Estimated Effluent TSS Conc.	169.75	mg/L	30% removal, 2002 EPA OWTS Manual

Table 7. Primary Settling Tank Specification

4.2 Membrane Bioreactor Units

A preliminary design was based around the SP400 Submerged Membrane Unit (SMU). Kubota's SP series of SMUs offer state-of-the-art technology. The SP series was developed in 2011 to create a Submerged Membrane Unit which is more energy efficient and faster to assemble on-site then the preceding RM/RW

series, while still maintaining the reliability and simplistic operation that is characteristic of Kubota's MBR systems. An overview of the structure of the SP series is provided below.



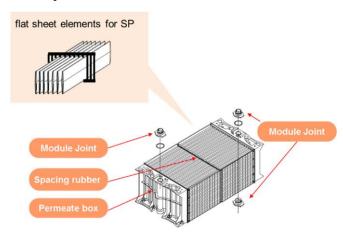


Figure 1. SP Series Unit Structure

Figure 2. MBR Module

One main takeaway is the cartridge structure of the SP series units, which differs from previous Kubota products. Forty individual membrane sheets are permanently fixed to each membrane module. Each module includes a permeate box and module joint on both ends. These modules are connected in a tubeless configuration by the integrated module joints to form a single cassette. Built-in retainers connect the assembled cassette to a permeate manifold which is connected to the permeate header. The SP series is suited for medium to large installations and offers fast assembly, easy maintenance, and up to 15% lower energy use for air scour in the MBR than other Kubota systems. An overview of the assembly and module connection is displayed below.

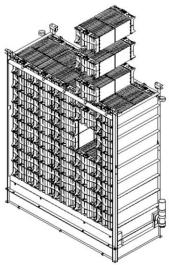


Figure 3. SP Series Module Assembly

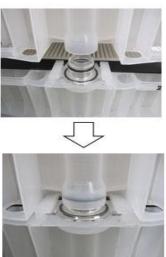


Figure 4. Module Connection Detail

Kubota's membrane sheet is made from chlorinated polyethylene with an average pore size of 0.2 micron (maximum 0.4 micron). This membrane is much thicker than other membranes to provide long-lasting durability and features high porosity to enable high flows. This pore size has been designed as the optimum balance between water quality and quantity and will be a great option for the proposed flow of the new WWTP.

Each MBR uses the process of activated sludge (secondary treatment) and membrane filtration (tertiary treatment). Membrane units are installed in the activated sludge reactor, where sludge and treated water are separated by means of physical filtration. MBRs eliminate the need for gravity sedimentation that are required for conventional activated sludge (CAS), thereby eliminating the need for final clarifiers. **Figure 5** compares the CAS process with the MBR process.

Conventional Activated Sludge (CAS) **MLSS** $(0.2 \sim 0.4\%)$ SS Leakage Influent Effluent Aeration Tank Sedimentation Tank Discharge Tank Equalization Excess Sludge Tank Sludge Thickener Kubota MBR MLSS Clean Effluent $(1.0 \sim 2.0\%)$ Influent Effluent Equalization MBR Discharge Tank Excess Sludge Tank

Figure 5. Typical CAS Process (top) vs. Kubota MBR process (bottom)

The Kubota SP series can operate at mixed liquor concentrations ranging from 5,000 mg/L to 13,000 mg/L, which is much higher than that of a conventional activated sludge basin. This allows the system to withstand influent load fluctuations and reduces aeration and waste sludge volume.

The primary method of membrane cleaning for the Kubota MBR system is the air scour provided by the diffusers at the base of the membrane units. The chemical cleaning system eliminates the need for separate tanks or tank linings for immersive cleaning. The system consists of a venturi injector which feeds the cleaning solution through the permeate piping using municipal utility water. The venturi system can be skid-mounted on a wall, as displayed below.

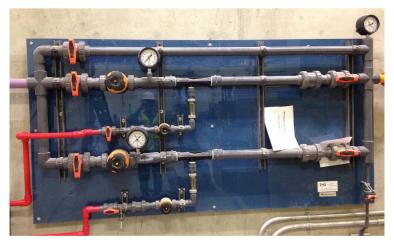


Figure 6. Skid-Mounted Clean-In-Place System

The cleaning process involves stopping the operation, opening a vent, injecting a chemical solution, and allowing that solution to soak in the membrane units for 2 to 4 hours.

Organic fouling can be cleaned with a 0.5% sodium hypochlorite (NaClO) solution two-four times a year. Inorganic fouling such as iron or aluminum can be cleaned by a 1% oxalic or citric acid solution once a year. If the residual chemical cannot be discharged from the system, it can be sent back to the raw water inlet or to the bioreactor to be neutralized. No recovery cleaning is necessary for operation of the Kubota MBR system.

Organic Compounds and Suspended Solids Treatment (BOD and TSS removal)

To meet nutrient level requirements, the influent concentrations were applied to the maximum monthly flow for determination of biological process volumes. **Table 8** below displays the anticipated effluent volumes using the MBR treatment process from the Kubota MBR proposal.

Table 6. Influent and Lindent volumes					
Constituent	Max Month Influent	Anticipated Effluent Limit			
	Concentration				
Biological Oxygen Demand (BOD)	154.35 mg/L	<5 mg/L			
Total Suspended Solids (TSS)	169.75 mg/L	<10mg/L			
TKN*	45 mg/L	-			
Total Phosphorus (P)	8 mg/L	<1 mg/L			
Total Nitrogen (N)	-	<10 mg/L			

Table 8. Influent and Effluent Volumes

According to the Kubota MBR design standards, the MBR system is designed to be capable of treating the maximum monthly flow for up to 3 months, peak daily flow for up to 24 hours, and peak hourly flow for up to 4 hours.

As calculated in **Table 7**, the influent concentrations of BOD and TSS into the MBR system after the septic tank will be 154.35 mg/L and 169.75 mg/L. Assuming each MBR unit treats equal amounts of BOD and TSS simultaneously, **Table 9** breaks down the percent removal rate of a MBR unit.

Constituent	Influent Load (lbs/day) per MBR Unit	Anticipated Effluent Limit (lbs/day) per MBR Unit	Percent Removal per MBR Unit
Biological Oxygen Demand (BOD)	18.68	<0.605	96.8%
Total Suspended Solids (TSS)	20.54	<1.21	94.1%
Total P	1.21	< 0.121	90.0%

Table 9. MBR Units Calculation

After the waste has been processed in the septic tank, each MBR unit treats about 18.68 lbs/day of BOD, 20.54 lbs/day of TSS, and 1.21 lbs/day of P. Using the anticipated effluent limit values from **Table 8**, the percent removal of BOD and TSS of each MBR unit were calculated to be approximately 96.8% and 94.1%, respectively. The percent removal of P by each MBR unit is 90.0%. Assuming that there will need to be removal of N and P, the anticipated effluent limits for P and N are predicted to be well below the draft effluent limit (DEL). The efficient removal of nutrients makes the Kubota MBR system a favorable option for the proposed WWTP. The calculations for the percent removal are shown below:

Percent Removal per MBR Unit for BOD:

$$58,000 \ gallons = 219,553.88 \ L$$

$$Anticipated \ Effluent \ Limit \ per \ MBR \ Unit = \frac{5 \ mg/L}{4} = 1.25 \ mg/L$$

$$Influent \ load : 154.35 \frac{mg}{L} \times 219,533.88L = 33,885,054.378 \ mg = 74.71 \ lbs \ BOD$$

$$Influent \ load \ per \ MBR \ unit = \frac{74.71 \ lbs \ BOD}{4 \ MBR \ units} = 18.68 \ lbs \ BOD$$

$$Removal \ per \ MBR \ Unit = \frac{1.25 \frac{mg}{L} \times 219,533.88 \ L}{453,592 \ mg/lb} = 0.605 \ lbs/day$$

$$Percent \ Removal = 1 - (\frac{0.605}{18.68} \times 100) = 96.8\%$$

Percent Removal per MBR Unit for TSS:

Anticipated Effluent Limit per MBR Unit =
$$\frac{10 \ mg/L}{4}$$
 = 2.5 mg/L

Influent load : 169.75 $\frac{mg}{L}$ × 219,533.88L = 37,265,876.13 mg = 82.16 lbs TSS

Influent load per MBR unit = $\frac{82.16 \ lbs \ BOD}{4 \ MBR \ units}$ = 20.54 lbs TSS

Removal per MBR Unit = $\frac{2.5 \frac{mg}{L} \times 219,533.88 \ L}{453,592 \ mg/lb}$ = 1.21 lbs/day

Percent Removal = 1 - ($\frac{1.21}{20.54} \times 100$) = 94.1%

Percent Removal per MBR Unit for P:

Anticipated Effluent Limit per MBR Unit =
$$\frac{1 \, mg/L}{4}$$
 = 0.25 mg/L

Influent load : $10.0 \frac{mg}{L}$ × 219,533.88L = 2,195,338.8 mg = 4.84 lbs P

Influent load per MBR unit = $\frac{4.84 \, lbs \, BOD}{4 \, MBR \, units}$ = 1.21 lbs P

Removal per MBR Unit = $\frac{0.25 \frac{mg}{L} \times 219,533.88 \, L}{453,592 \, mg/lb}$ = 0.121 lbs/day

Percent Removal = $1 - (\frac{0.121}{1.21} \times 100)$ = 90.0%

Nitrification

Nitrification will occur combined with the BOD removal in each MBR unit. The effluent limit is anticipated to be <10 mg/L, meaning each MBR unit produces <2.5 mg/L of effluent. The Kubota MBR tank works as both a solid-liquid separation tank and an aeration tank. Kubota's stable air scour and infrequent chemical cleaning allows aeration from the air scour to be used as oxygen supply for biological treatment. This reduces the oxygen requirement in the aeration tank.

4.3. UV Disinfection System & Aeration

Treated effluent will enter a UV disinfection system before discharge into the creek. UV light can eliminate many microorganisms such as bacteria, protozoa, and harmful pathogens that are not eliminated by chlorine.

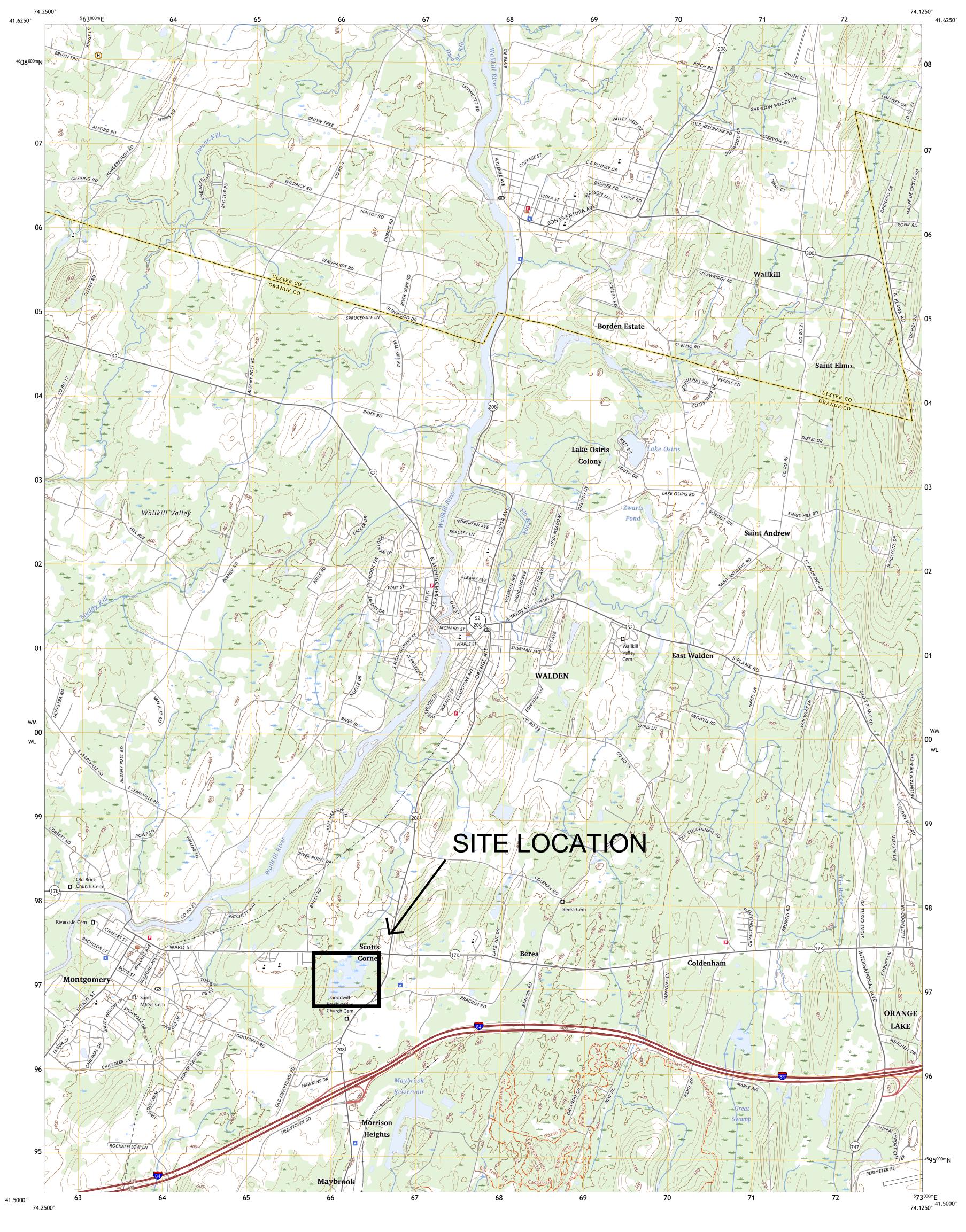
Re-aeration will be accomplished using MBR blowers with positive displacement at 6.7 psig. The re-aeration system will provide approximately 175 scfm of air to maintain an effluent DO concentration of > 5 mg/L. There will be two (2) MBR blowers on duty and one (1) on standby.

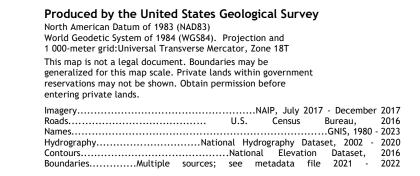
5. CONCLUSION

To provide successful wastewater treatment for the Sheffield Gardens project, a WWTP consisting of a 12,000-gallon septic tank for primary settling, a process train with a 6,730-gallon anoxic tank and two (2) 8,387-gallon MBR tanks operating in parallel for organics and solids removal. The WWTP will be capable of treating 58,000 gpd of wastewater to < 5mg/L of BOD and < 10 mg/L of TSS. Nitrogen and phosphorus levels will be below 10 mg/L and 1 mg/L, respectively. The effluent will then be disinfected though UV disinfection and re-aerated via MBR blowers before discharge into the wetland.

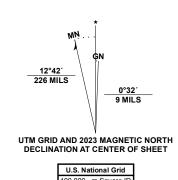
The treated wastewater is proposed to be discharged to the wetland connecting to a tributary creek of Wallkill River, where mitigations will be made to avoid encroaching onto the neighboring property.

Appendix A. Location Map





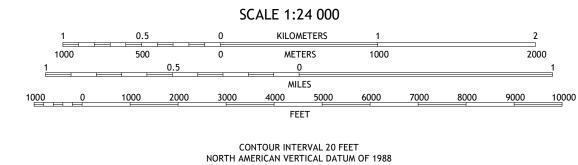
..FWS National Wetlands Inventory 1984 - 2011



WM

WL

Grid Zone Designation



This map was produced to conform with the National Geospatial Program US Topo Product Standard.



ADJOINING QUADRANGLES

4 Pine Bush 5 Newburgh

6 Goshen 7 Maybrook

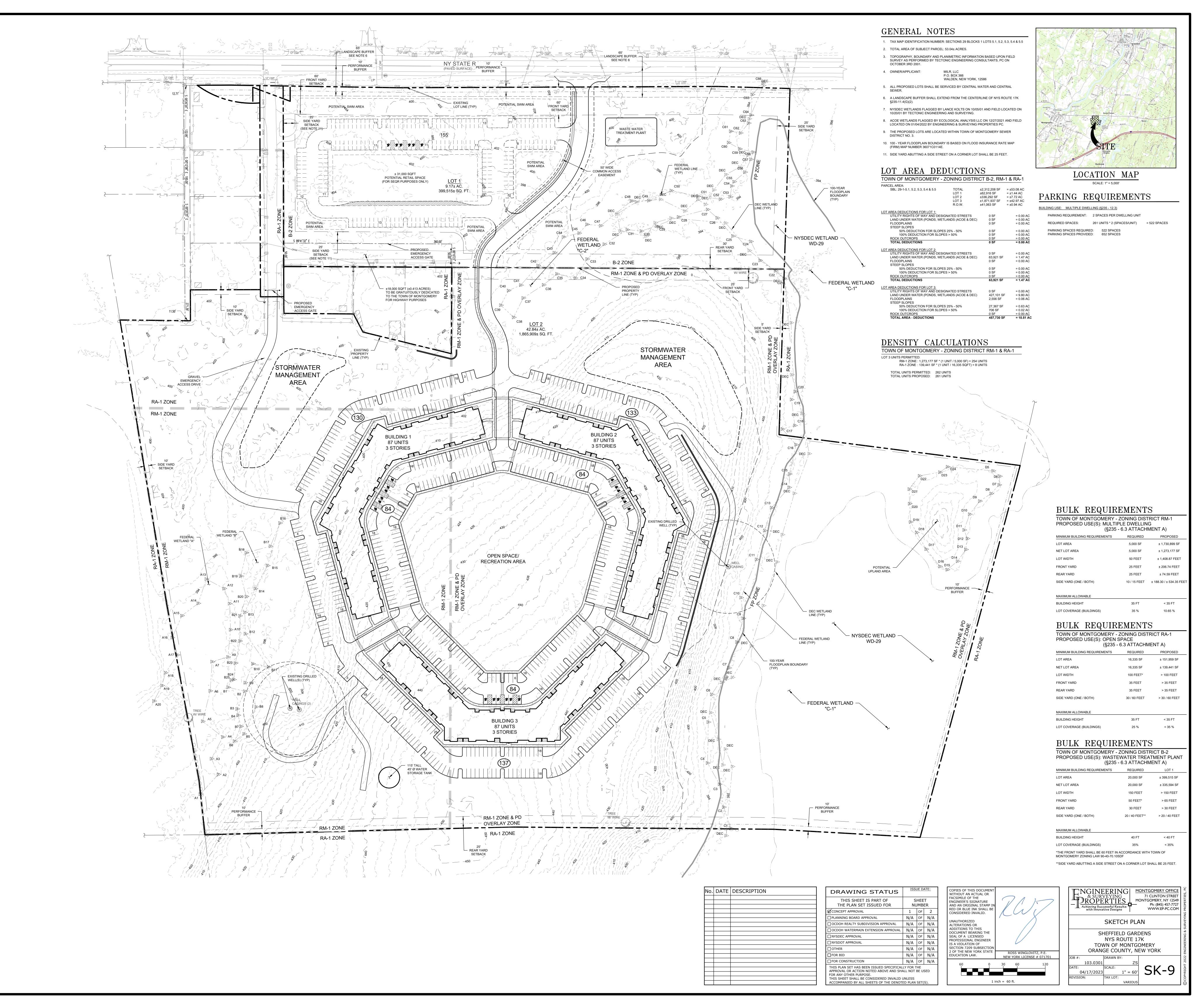
8 Cornwall-on-Hudson







Appendix B. General Site Plan



Appendix C. SPDES Permit



State Pollutant Discharge Elimination System (SPDES) Application Form: Private, Commercial & Institutional (P/C/I) Discharge of Treated Sanitary Sewage

New Application	○ Renewa	al Application	Modification Application
SPDES Number NY####		DEC Authoriza	#-####################################
Applicant/Owner Information		Contact/Agent	
Over a rabin.	ndividual	Name	
	ublic	Jason Pitingaro	
Name	Taxpayer ID	Title	
MILR, LLC		P.E., President	
Mailing Address		Mailing Address	
PO Box 366		15 Industrial Drive, Su	uite 2
City	te Zip	City	State Zip
Walden	12586	Middletown	NY 10941
Phone Email		Phone	Email
		845-703-8140	pitingaro@panddengineers.com
Facility Information			
Facility Name	Nature of	f Business or Facility	Population Served
Sheffield Gardens	Residenti	ial, Commercial	625
Street Address		City	State Zip
NYS Route 17k		Montgomery	NY 12549
Municipality M	unicipality Name		County
	own of Montgomery		ORANGE
Additional Facility Location Information			
SBL 29-1-5.1, 5.2, 5.3, 5.4 & 5.5			
Section Tax Map Information 29	Block	Lot 5.1, 5.2, 5.3, ∉	
Certification: I hereby affirmany attached supplemental forms herein are punishable as a Class	is true to the best	of my knowledge and	
1			

State Department of Environmental Conservation or its designated agency.

Please Indicate Whether Your Facility 'Discharges To Groundwater', 'Discharges To Surface Water', or both.					
Discharges To Groundwater					
Discharges To Surface Water					
SPDES Application for P/C/I	Discharge of Treated Sanitary Sewage				
Discharges To	o Groundwater - 1 of 1				
Facility Name Sheffield Gardens					
SPDES Number	DEC Authorization				
To Add or Remove outfalls, click on the Green	n + or the Red X respectively.				
Use additional copies of this page to list add	your facility has any discharges to groundwater. itional groundwater outfalls. Sampling information is ned to discharge, or discharges 30,000 GPD or more.				
Outfall Information:					
Outfall No. Outfall Status Proposed Replacement	Design Flow Existing Expansion Gal/Day				
Outfall Location (if subsurface Latitude system, indicate center of disposal system area) Longitude					
Treatment:					
Standard On Site Treatment: Septic Tanks with:	Alternative On Site Treatment: Septic Tanks with:				
☐ Absorption Trenches ☐ Cut and Fill Systems	Absorption Trenches Using An Alternative Aggregate Single-Pass Sand Filters & Pressurized Shallow Narrow Drainfields				
Shallow Absorption	Shallow Absorption Trenches Using An Alternate Mound Systems Aggregate				
☐ Absorption Beds ☐ Seepage Pits ☐ Absorption Beds Using An Alternate Aggregate ☐ Drip Dispersal or Other Low Profile Dispersal System					
Other (describe)					
Frequency of Discharge Months/Year Days/Week					
Name of Nearest Surface Waters Distan	ce Soil Type Depth To Water Table Ft. Ft.				

SPDES Application for P/C/I Discharge of Treated Sanitary Sewage <u>Discharges to Groundwater</u>

Facility Name	Sheffield Gardens		
SPDES Number		DEC Authorization	
Outfall No.			

Sampling Information

Include the following sampling information if the disposal system is designed to discharge, or discharges, 30,000 GPD or more. Please indicate whether the values listed are from sampling results (include the date), estimated from the treatment system design as installed, or estimated from the proposed treatment system design.

Plant Design Pollutant Information	Influent		Effluent		Number of Samples or Source of Estimate
	mg/l	lbs/day	mg/l	lbs/day	
BOD5					
Percent removal, BOD5					
pH, Range					
Nitrate, as N					
Nitrite, as N					
Ammonia, as N					
Nitrogen, Total, as N					
Phosphorus, Total, as P					
Total Residual Chlorine, if used					
Solids, Total Dissolved (Nassau/Suffolk only)					

SPDES Application for P/C/I Discharge of Treated Sanitary Sewage Discharges To Surfacewater - 1 of 1

Sheffield Gardens

Wetland (WD-29) connecting to MINOR TRIBS TO MIDDLE WALLKILL

Facility Name

SPDES Number	DEC Authorization						
To Add or Remove outfalls, click on the Green + o	To Add or Remove outfalls, click on the Green + or the Red X respectively.						
Complete this page of the application if your Complete this form for ea	facility has any discharges to surface water. ach surface water outfall.						
Discharge Data							
Outfall No. Outfall Status Proposed Replacement CE	Design Flow Existing © Expansion 58,000 Gal/Day						
Outfall Location (end of pipe or conveyance) Latitude 41							
Type of Treatment							
MBR treatment with Nitrogen and Phosphorus removal utilizing an anoxic tank, MBR tanks, UV disinfection, and discharge.							
Frequency of Discharge Months/Year 12 Day	rs/Week 7						
Name of Receiving Water	Classification Water Index Number						

С

H-139-13-20 thru 53

SPDES Application for P/C/I Discharge of Treated Sanitary Sewage <u>Discharges to Surface Water</u>

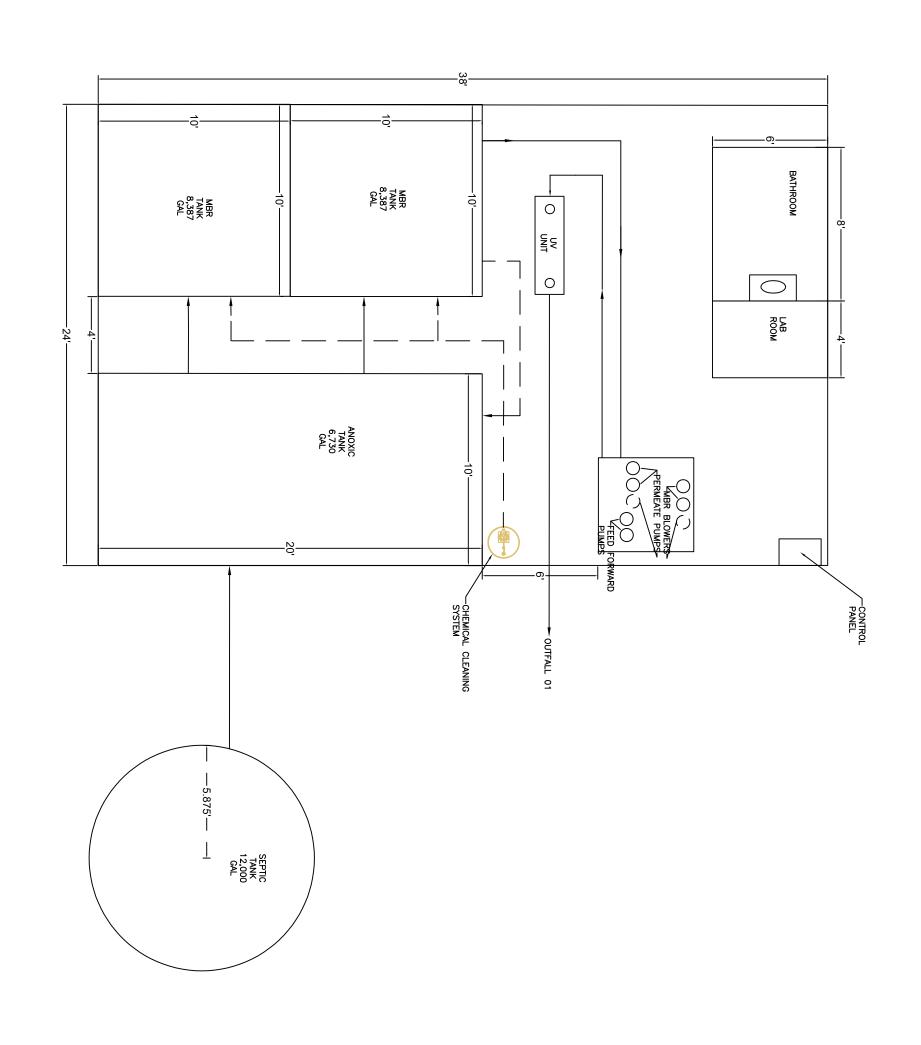
Facility Name	Sheffield Gardens		
SPDES Number		DEC Authorization	
Outfall No. 001			

Sampling Information

Include the following sampling information. Please indicate whether the values listed are from sampling results (include the date), estimated from the treatment system design as installed, or estimated from the proposed treatment system design.

Plant Design Pollutant Information	Infl	uent	Effluent		Number of Samples or Source of Estimate
	mg/l	lbs/day	mg/l	lbs/day	
BOD5	250		<5		estimated
Suspended solids	250		<10		estimated
Percent removal, BOD/TSS	/		98/96		estimated
pH, Range	/		/		
Settleable solids, ml/l	/		/		
Solids, total dissolved	/		/		
Dissolved oxygen	/		/		
Ammonia, as N	/		/		
Nitrogen, Total, as N	/		<10		estimated
Phosphorus, Total, as P	8		<1		estimated
Fecal Coliform, MPN	/		/		
Total Residual Chlorine (if used)	/		/		
Temperature, Degrees F, Summer	/		/		
Temperature, Degrees F, Winter	/		/		

Appendix D. WWTP Layout



EACH SHEET IS INCOMPLETE OR INVALID UNLESS ACCOMPANIED BY ALL THE SHEETS IN THE SET.

IT IS A VIOLATION OF NYS EDUCATION LAW SECTION 7209 FOR ANY PERSON, UNLESS THEY ARE ACTING UNDER THE DIRECTION OF A LICENSED PROFESSIONAL ENGINEER, LAND SURVEYOR, OR ARCHITECT TO ALTER AN ITEM BEARING THE STAMP OR SEAL OF A LICENSED PROFESSIONAL IN ANY WAY. IF AN ITEM IS ALTERED, THE ALTERING ENGINEER, LAND SURVEYOR, OR ARCHITECT SHALL AFFIX TO THE ITEM THEIR STAMP OR SEAL AND THE NOTATION "ALTERED BY" FOLLOWED BY THEIR SIGNATURE, THE DATE OF SUCH ALTERATION, AND A SPECIFIC DESCRIPTION OF THE ALTERATION.

CONTRACT NO.

230014

1 OF 1

WWTP LAYOUT

WWTP LAYOUT

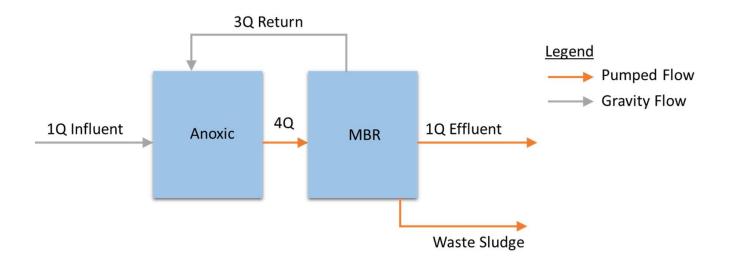
SHEFFIELD GARDENS TOWN OF MONTGOMERY ORANGE COUNTY, NEW YORK

SHEET NO. 1 O	_F 1	Each sheet is incomplete or invalid	DATE:	REVISION:	BY:
SILETINO. OI		unless accompanied by all the sheets			
SCALE: AS SHOWN	DRAWING NAME:	in the set.			
SHOWN		It is a violation of NYS Education Law Section 7209 for any person, unless			
DATE: 12/22/2023	WWTP LAYOUT	they are acting under the direction of a licensed professional engineer, land			
		surveyor, or architect to alter an item bearing the stamp or seal of a			
JOB NO.: 230014	DRAWN BY: LL	licensed professional in any way. If an item is altered, the altering engineer,			
FOR REVIEW &		land surveyor, or architect shall affix to the item their stamp or seal and the			
COMMENT	FOR APPROVAL	notation "altered by" followed by their signature, the date of such alteration.			
FOR BID & CONSTRUCTION	AS-BUILT	and a specific description of the alteration.			
CONSTRUCTION	\smile				

PITINGARO & DOETSCH CONSULTING ENGINEERS, P.C

15 INDUSTRIAL DRIVE SUITE 2 MIDDLETOWN, NEW YORK 10941 PH: 845 703-8140 FAX: 845 703-8143 INFO@PANDDENGINEERS.COM WWW.PANDDENGINEERS.COM

Appendix E. Flow Diagram of Treatment Process



Appendix E. Process Flow Schematic

Appendix F. MBR Equipment Information

Name	Туре	Anticipated Size	Quantity		
Headworks Zone Equipment					
Fine Screen	Internally Fed Drum	100 gpm	1		
Anoxic Zone Equipment					
Anoxic Mixer	Submersible	12,000 gal	2		
Level Switch	Float	-	2 (1 HL + 1LL)		
Level Transmitter	Hydrostatic	-	1		
	Membrane Equipme	nt			
Submerged Membrane Unit	Flat Plate, 304 stainless steel housing	SP225	4		
Guide Set	Kubota	-	4 sets		
Level Switch	Float	-	2 LL		
MBR Blower	Positive Displacement	175 scfm 6.7 psig	2 duty + 1 common standby		
Air Flow Meter	Mass Air Flow, Insertion style	-	2		
Permeate Pump	Self-Priming Centrifugal	50 gpm	2 duty + 1 standby		
Permeate Flow Meter	Electromagnetic	2-inch	2		
Permeate Turbidity Meter	Optical Meter and Transmitter	-	1		
Permeate Pressure Transmitter	Diaphragm	-	1		
WAS Pump	Self-Priming Centrifugal	20 gpm	1 duty		
WAS Pump Flow Meter	Electromagnetic	1-inch	1		
Feed Forward Equipment					
FF Pump	Submersible	150 gpm	1 duty + 1 standby		
FF Pump Flow Meter	Electromagnetic	3-inch	1		
Other Equipment					
Alum Addition System	Dosing Pump, Calibration Column, Injection Quill	-	1 system		
CIP System	Chemical Injection System	-	1 system		
Control Panel, HMI, SCADA	MBR Control Panel	-	1		
Process Tanks	Precast Concrete	10′ X 20′ X 12′	2		

Appendix F. Major Equipment and Instrumentation of MBR Treatment